# Mild-catalytic conversion toward diluent reduction

Developing an actionable path to partial upgrading at site

**NEXT**STREAM<sup>®</sup>

### NPUC Workshop - May 26, 2022

- Introduction to NextStream
  - The team
  - The technology
  - Our approach to reducing bitumen viscosity in the field
- Technical Discussion
  - Compare the NextStream catalytic approach to a thermal-only mechanism
  - Equivalent conversion basis 90% viscosity reduction
- Analytical Analysis to Provide Insight into Mechanism?
  - Whole crude sample analysis
  - XPS analysis of asphaltene
  - Is there a simple mechanistic explanation?
- Brief Look at Viscosity Reduction in the Field

## **NextStream Heavy Oil – The Team**

- 10 years of fundamental research and development
  - Joint effort between Baker Hughes and Rice University
  - Considerable thought, design and effort from the outset
- Spun out under the NextStream umbrella in 2018
  - Autonomous, self-directed team
  - Baker Hughes retains minority ownership
  - Provides operations support
- Currently scaling proprietary technology, moving from the laboratory into the field



Sivaram Pradhan, Ph.D. Catalyst R&D



Amin Haghmoradi, Ph.D. Process engineering



Mike Shammai, B.Sc. Reservoir dynamics Baker Hughes Fellow (1958-2021)



Manjusha Verma, Ph.D.

Analytical chemistry

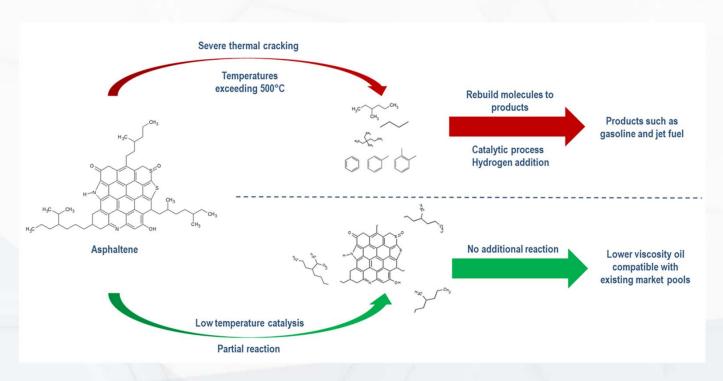


Wade Bullock Equipment & process engineering



Jacob Gibson, Ph.D.
Partial upgrading
technology evaluation

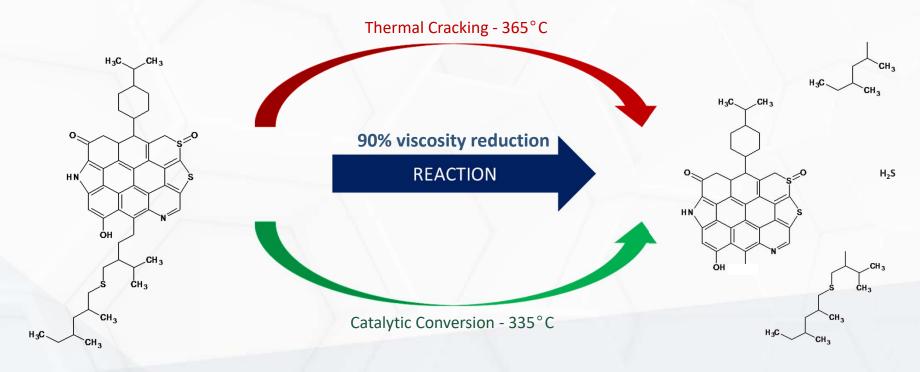
#### Well-designed Catalysts Allow Low-temperature Conversion



# Benefits of low-temperature reaction are many:

- Lower consumption of natural gas hence, lower GHG emission profile
- Minimal thermal cracking, thereby eliminating the formation of coke and olefinic material – avoids the need for post-processing hydrotreatment
- Simplified process allowing for seamless integration into existing SAGD facilities

## Today's Discussion: Catalytic vs. Thermal Reaction

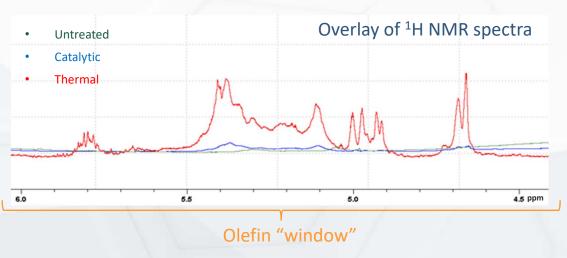


In both cases, equivalent conversion (viscosity reduction) sought for comparison

### Whole Sample Analysis – Equivalent Conversion

\*Analysis conducted by 3<sup>rd</sup> party laboratory

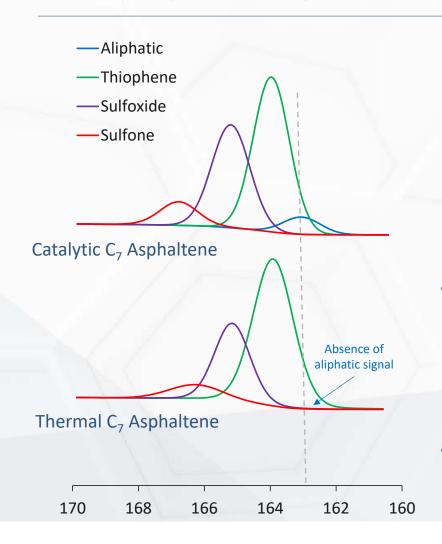
	Viscosity (30°C)	Olefin (%)*	P-Value*	Sulfur*	Asphaltene (%)
Untreated	140,000 cP	<0.30%	2.6	5.1	14.6
Catalytic	14,700 cP	<0.30%	2.2	4.7	11.8
Thermal	14,500 cP	0.80-0.90%	1.6	4.6	11.8



- Most notable, is the onset of olefins detected in the thermally-cracked sample
- P-Value substantially higher for the catalytically processed material
  - Suggests increased asphaltene stability
- Similar decline in both sulfur and asphaltene content
  - Not necessarily chemical modification of asphaltene molecules
  - Possible increased solubility in greater hydrocarbon matrix



#### **XPS Analysis of Asphaltene Fraction**



		*XP:			
	Aliphatic	Thiophenic	Sulfoxide	Sulfone	
Untreated	66.1%	33%			
Catalytic	5.2%	57.8%	33.9%	3.0%	
Thermal	4 <u></u> - N	63.2%	34.6%	2.1%	
Cat <sub>Field</sub>	1.9%	62.3%	34.9%	1.0%	95% visc. reduction
	S	S	S		
BE 1	66.8 eV BE 165.3	B eV BE 164.2 eV	BE 162.7 e	V	

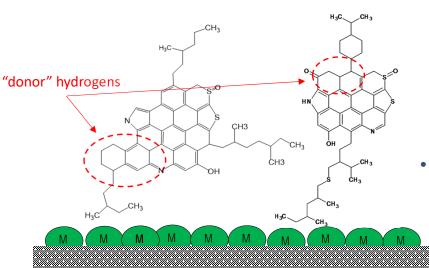
- Complete absence of aliphatic sulfur in thermally cracked product
  - Supports NextStream catalytic approach as more "mild"
  - Also suggests additional mechanism of conversion, which does not involve C-S bond
- Unlikely that significant thiophenic sulfur is being converted, but requires further analysis

#### Differences Between Mild-catalytic and Thermal Approaches

- Primary difference is the significant amount of olefin generation under higher temperature
  - High olefin content (~1.0%) limits the deployment of thermal cracking/visbreaking at site
  - Lower temperature + catalyst approach yields substantial viscosity reduction with little-to-no-olefin generation
  - Does not require post-reaction hydrotreatment, thereby simplifying the partial upgrading process at site
- Product maintains much of its stability as evidenced by P-Values above 2.0
  - Thermal cracking processes quickly reach a P-Value near 1.3, where stability and blendability with other crudes becomes problematic – again, limiting their deployment as a primary mechanism
- Preliminary XPS evaluation of the processed asphaltene fractions identifies significant differences
  - Mild-catalytic approach does not completely eliminate aliphatic sulfur bonds, suggesting a less "aggressive" approach
  - Given that both approaches achieve equivalent viscosity reduction, the catalytic process must introduce an additional, non C-S chemical reaction.



#### **Increased Hydrogen Donation from Tetralin-like Features**



- Catalyst surface designed to interact with structural moieties present in asphaltenes
  - Asphaltenes often associated with high "tetralin-like" features, or "hydrogen donor" capability
  - High asphaltene density at catalyst surface increases the frequency of hydrogen donation to terminate free radical reactions leading to an aromatic product vs. olefinic

#### Pseudo concentration affect

 similar to removing free radical access to paraffinic or alkyl "donors", which eliminate to form single or double carbon-carbon double bonds

#### A Brief Look at Performance in the Field





- Prototype system contains the following components:
  - "Inverted" emulsion separator provides diluent-free bitumen feed
  - Reactor section contains 4 catalyst-packed "pipes" in series configuration
  - Post-reaction heat exchange to preheat feed to the system
  - Substantial instrumentation and sampling capabilities
- Performance KPI's
  - Viscosity
    - Bitumen 1,138,000 cP (15°C)
    - Product 49,000 cP 80,600 cP (15°C)
  - Olefin content
    - 95% viscosity reduction achieved with no detectable olefins (<0.3%)
    - As high as 0.6%
- Quality improvements
  - TAN < 1.0
  - 15% reduction in vacuum residue IBP remains close to 200°C

# Thank you

